



## TWO-PHASE FLOW IN A POROUS MEDIA

## TEST-CASES PERFORMED WITH TOUGH2

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# Tough2 – Overview (1/2)

- **Code for multi-phase and multi-component fluid flow and transport in porous media**
- **Developed at Lawrence Berkeley National Laboratory (LBNL)**
- **Thermophysical fluid properties for a wide range of pressures and temperatures**
- **Many capillary pressure and relative permeability relationships**
- **Available version with FORTRAN 77 files of source code =>adaptable for specific needs:**
  - » additional relationships (Problem4)
  - » additional outputs
- **Specific fluid property modules:**
  - » EOS5 for water/hydrogen mixtures (Problems 1-2-3)
  - » EOS3 for water/air mixtures (Problem 4)

## Tough2 – Overview (2/2)

- Space discretization is made from the integral form of the basic conservation equations (IFDM: integral finite difference method)
- Time is discretized fully implicitly (first-order)
- Linear equation system is solved using a Newton-Raphson iteration process
- Automatic time step control
- Primary variables (isothermal conditions):
  - » single phase conditions:  $P$ ,  $X_{\text{mass H2/air}}$
  - » two-phase conditions:  $P_g$ ,  $S_g$
  - » primary variables are switched and re-initialized in response to a change of phase

## Tough2 modules EOS3/EOS5

- Components: water and hydrogen (EOS5) or air (EOS3)
- Phases: liquid and gas
- Ideal gas law for gas phase
- Dalton's law for partial pressures:  $P_{\text{gas}} = P_{\text{H}_2/\text{air}} + P_{\text{vap}}$
- Fluid advection described with a multiphase extension of Darcy's law
- Solubility of hydrogen according to Henry's law:  $X_{\text{mole}} = H * P_{\text{H}_2/\text{air}}$

# Main deviations from the test-cases specifications

## ➤ Diffusion model:

» diffusive flux  $j_\alpha^i$  of component i in fluid phase  $\alpha$

$$j_\alpha^i = -\phi S_\alpha \rho_\alpha d_\alpha^i \nabla X_\alpha^i$$

with  $X_\alpha^i$  mass fraction of component i in phase  $\alpha$

## ➤ Vapor pressure is not neglected:

» At 300 K saturated vapor pressure is 3532 Pa

» At 303 K saturated vapor pressure is 4205 Pa

## ➤ Compressibility of liquid water

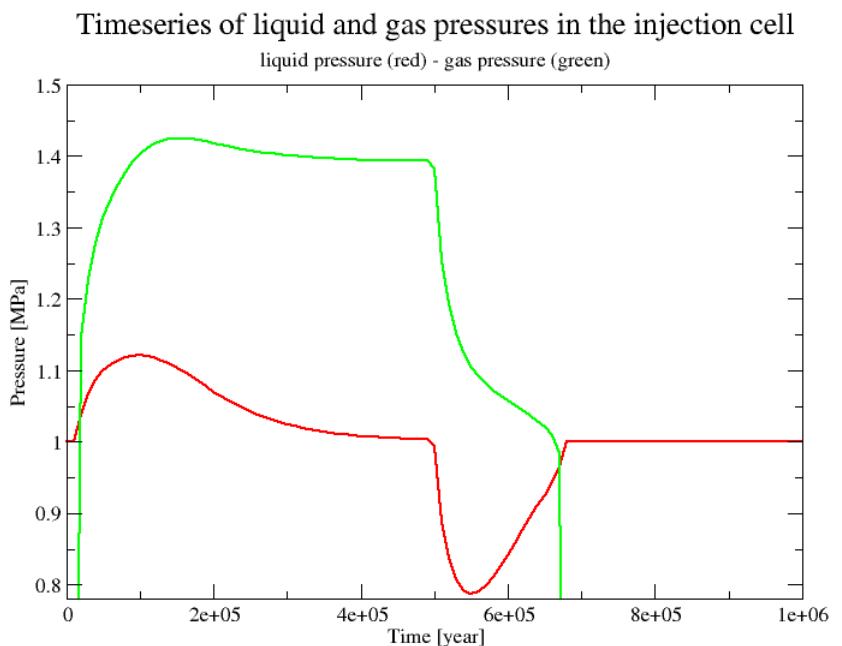
## ➤ Production term for hydrogen:

» applied on a thin specific volume instead of a boundary surface

# Problem 1: gas phase appearance/disappearance

- Porous media initially fully saturated with pure water

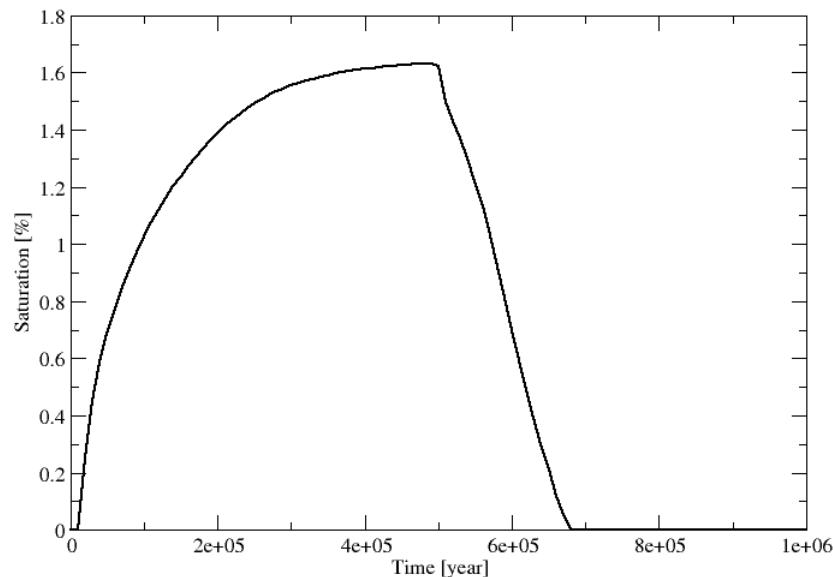
- Regular spatial discretization:  $dx=1$  m
- Time discretization:
  - »  $dt_{min}=1$  s,  $dt_{max} = 1000$  years
- Relative convergence criterion:  $10^{-5}$



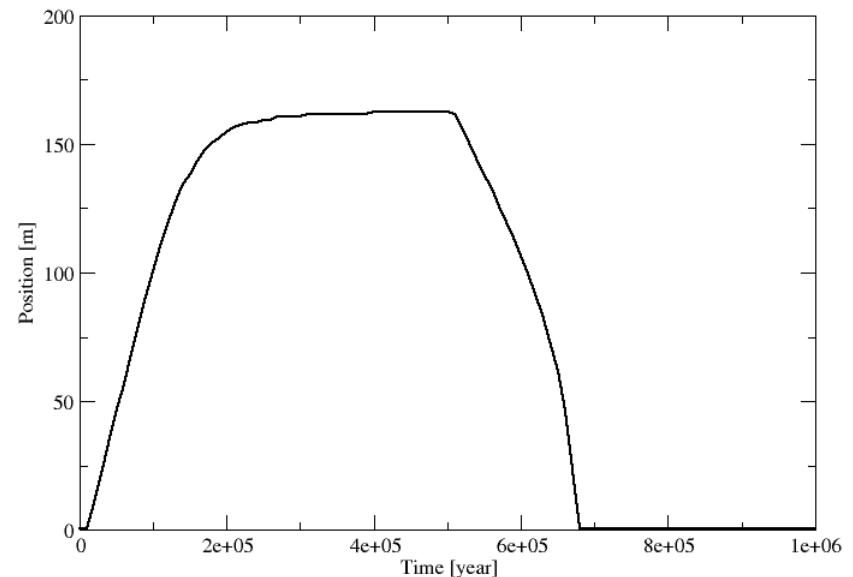
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Timeseries of gas saturation in the injection cell

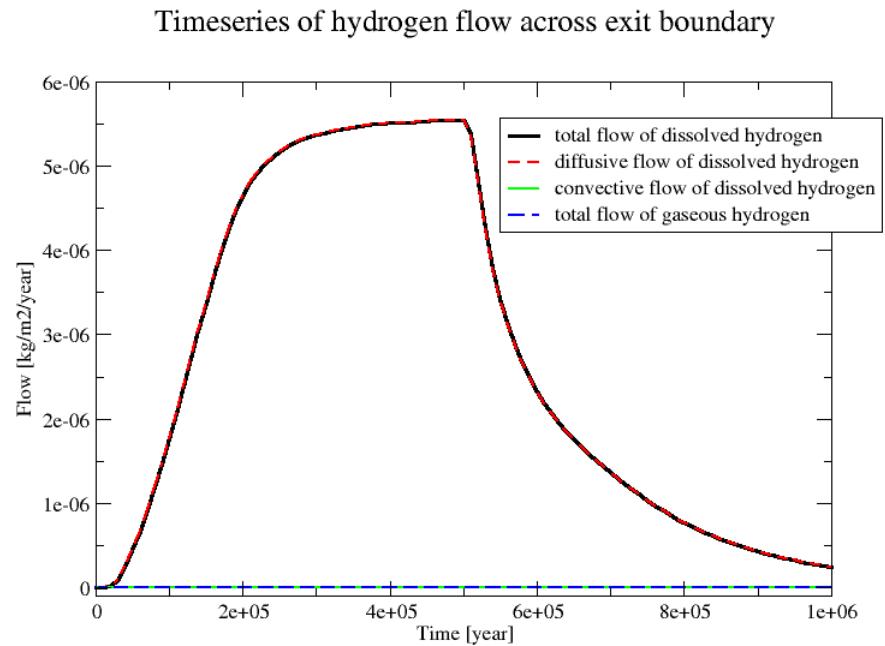
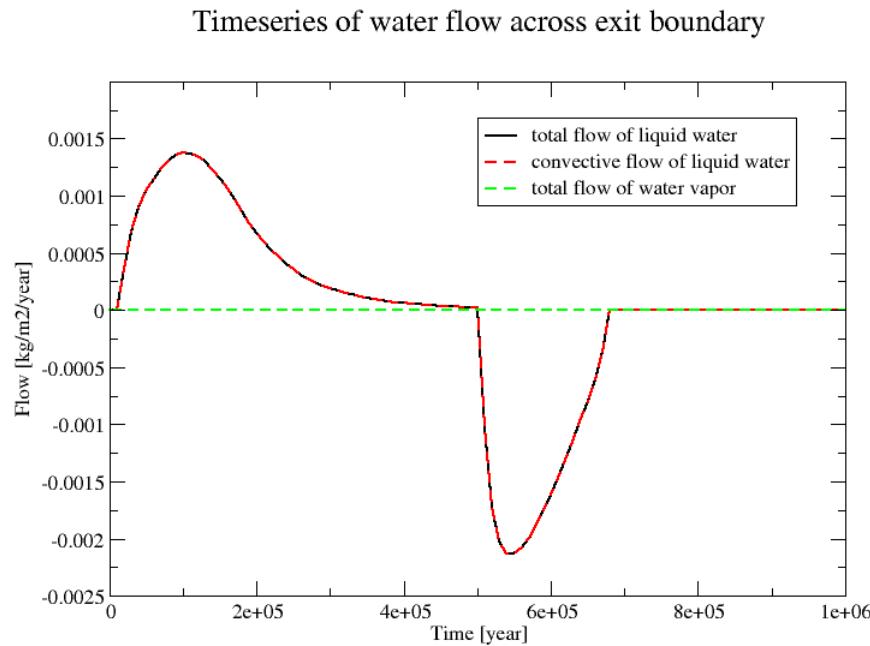


Timeseries of saturation front position



# Problem 1: gas phase appearance/disappearance

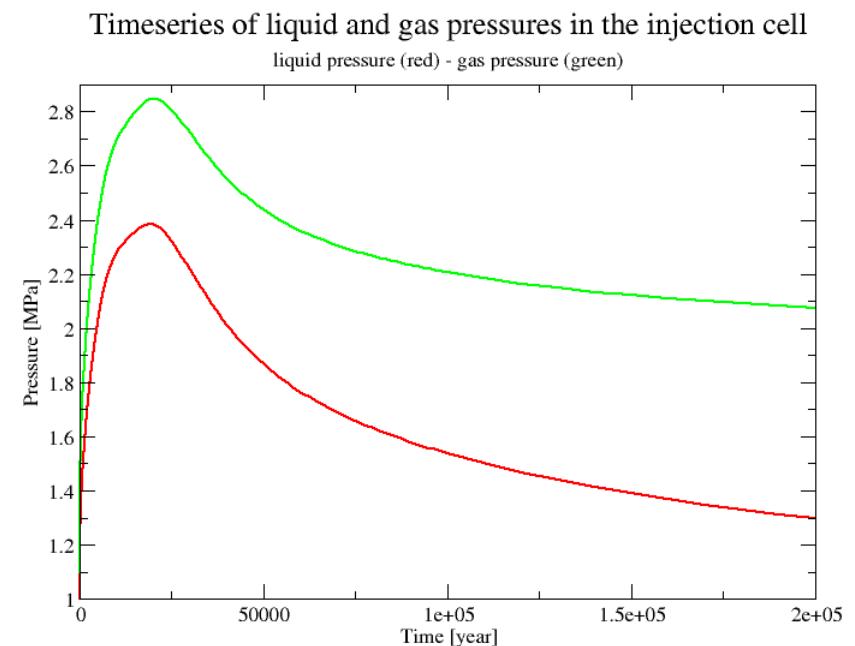
➤ Porous media initially fully saturated with pure water



# Problem 1: gas phase appearance/disappearance

- Porous media initially partially saturated with liquid

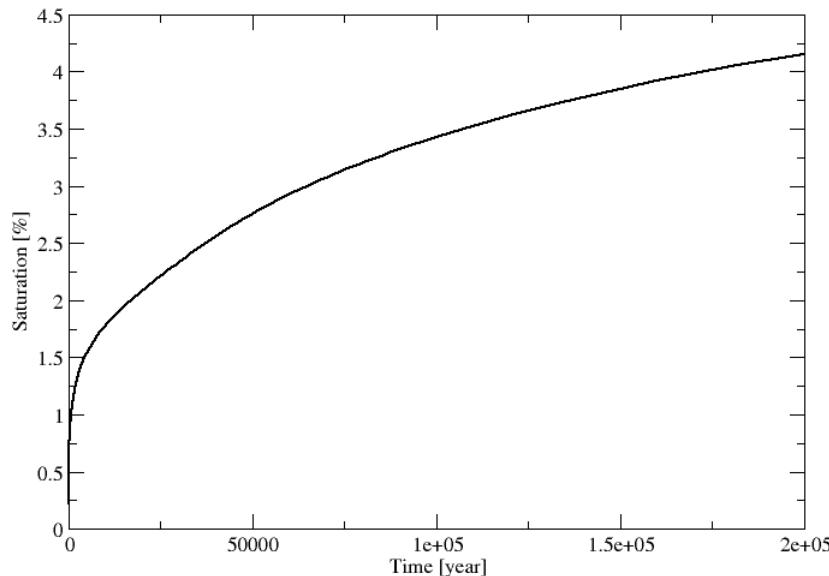
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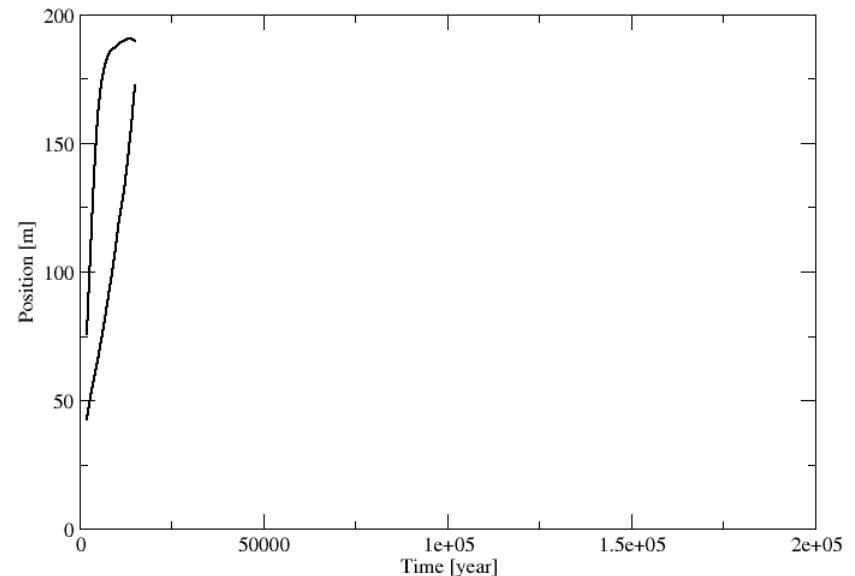
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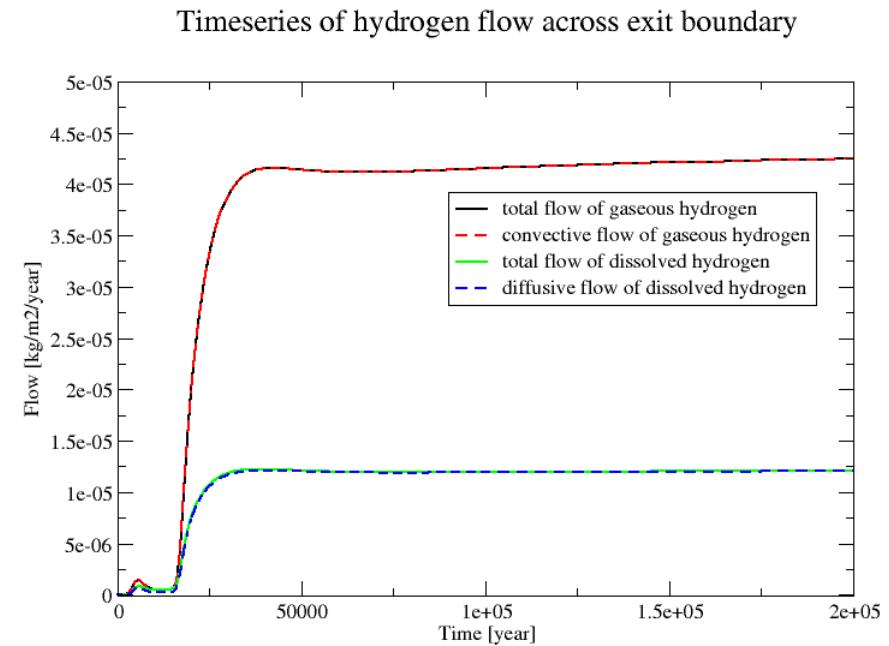
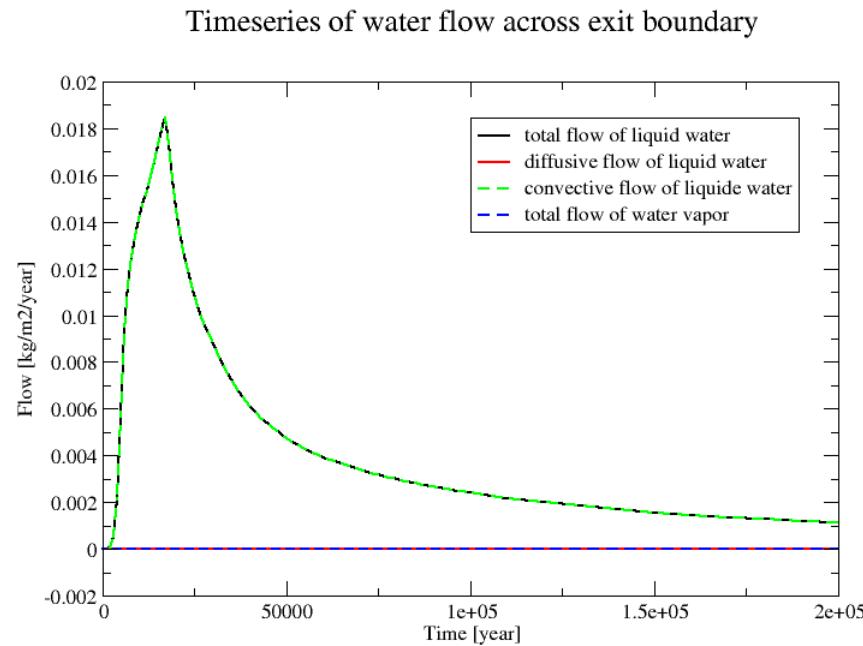


Timeseries of saturation front positions



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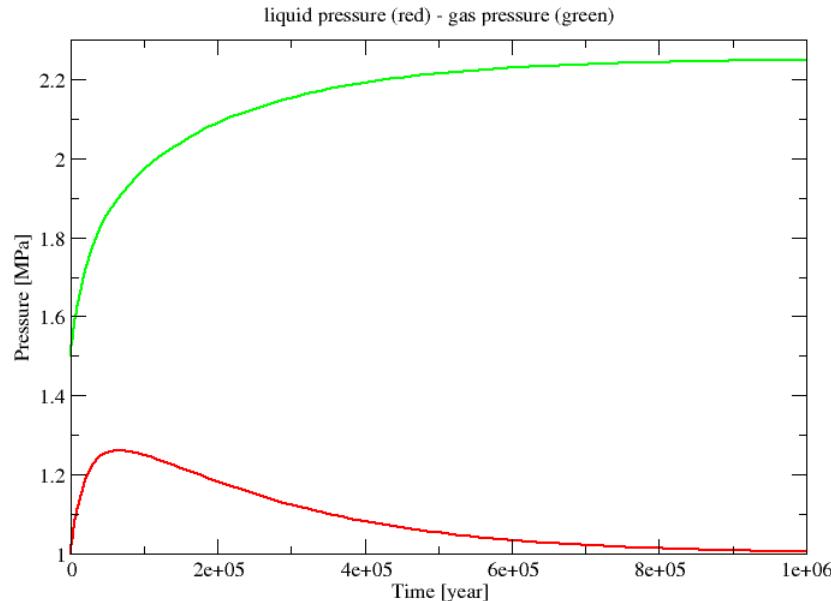
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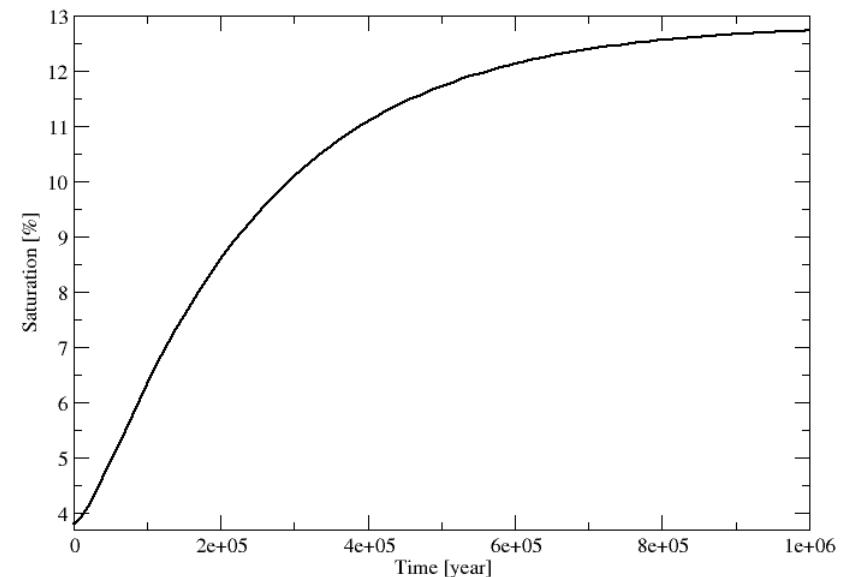
# Problem 2: two-phase flow in a non homogeneous porous media

## ➤ Porous media initially partially saturated with liquid

Timeseries of liquid and gas pressures in the injection cell



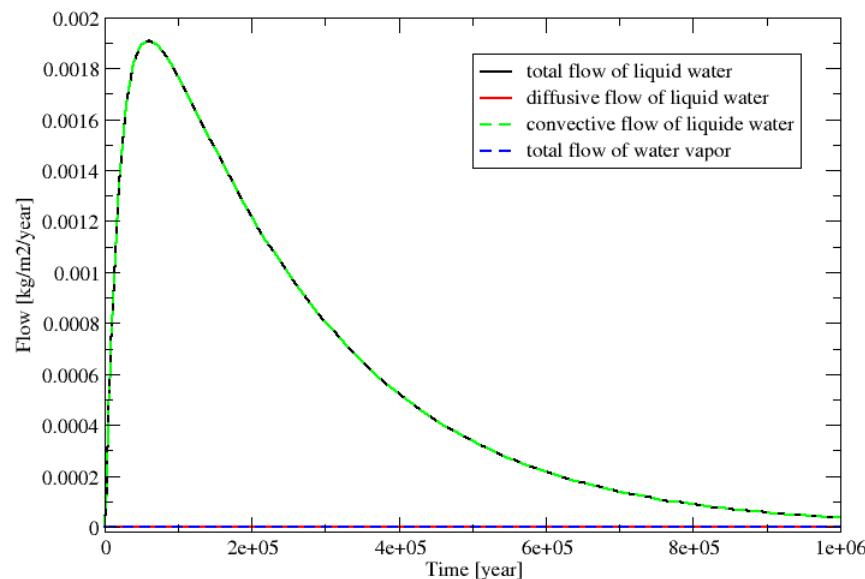
Timeseries of gas saturation in the injection cell



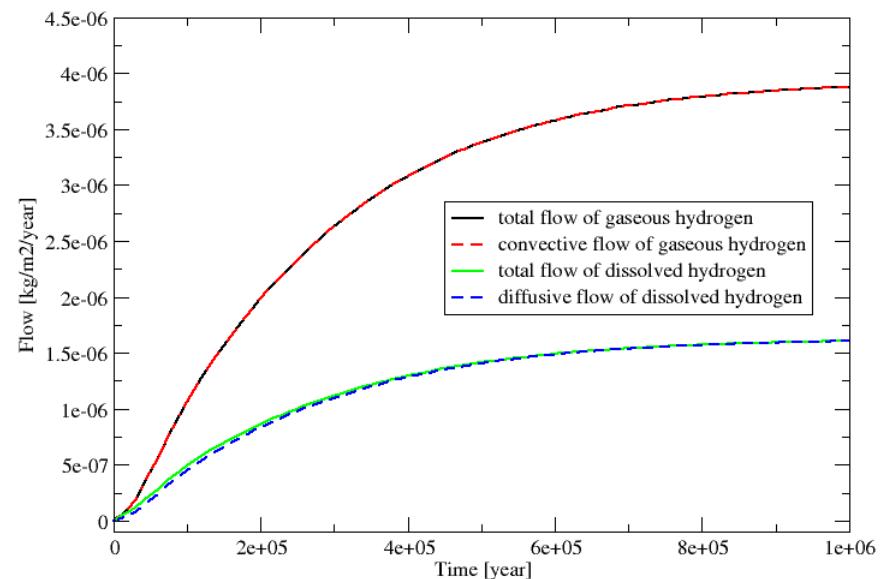
# Problem 2: two-phase flow in a non homogeneous porous media

## ➤ Porous media initially partially saturated with liquid

Timeseries of water flow across exit boundary



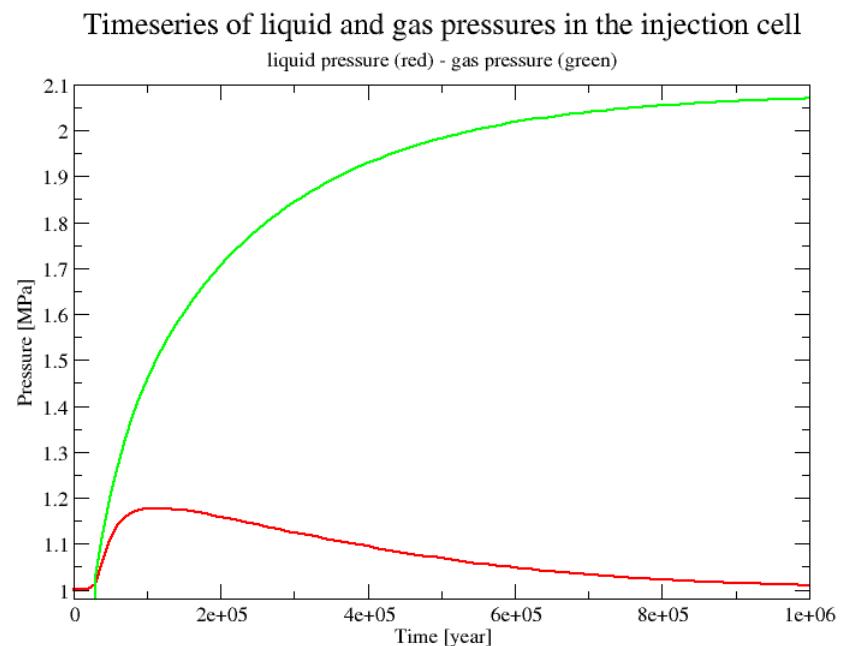
Timeseries of hydrogen flow across exit boundary



## Problem 2: two-phase flow in a non homogeneous porous media

- Porous media initially fully saturated with pure water

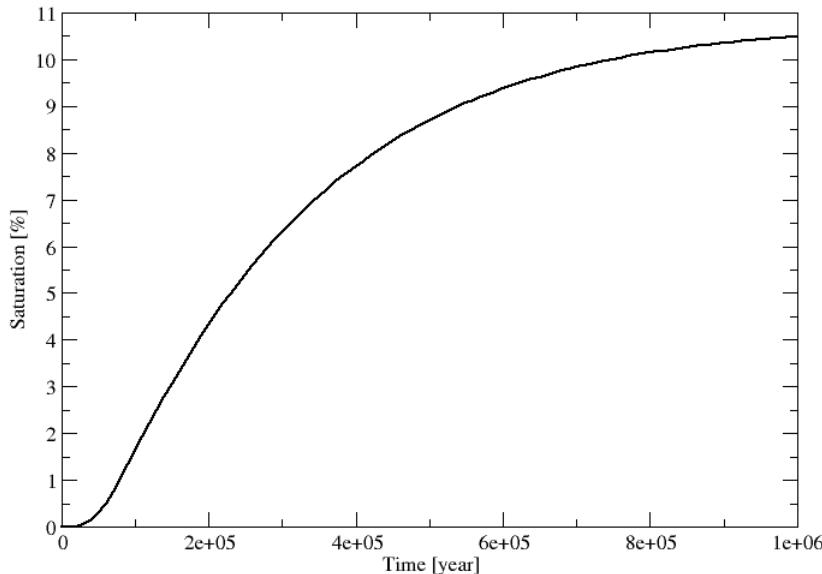
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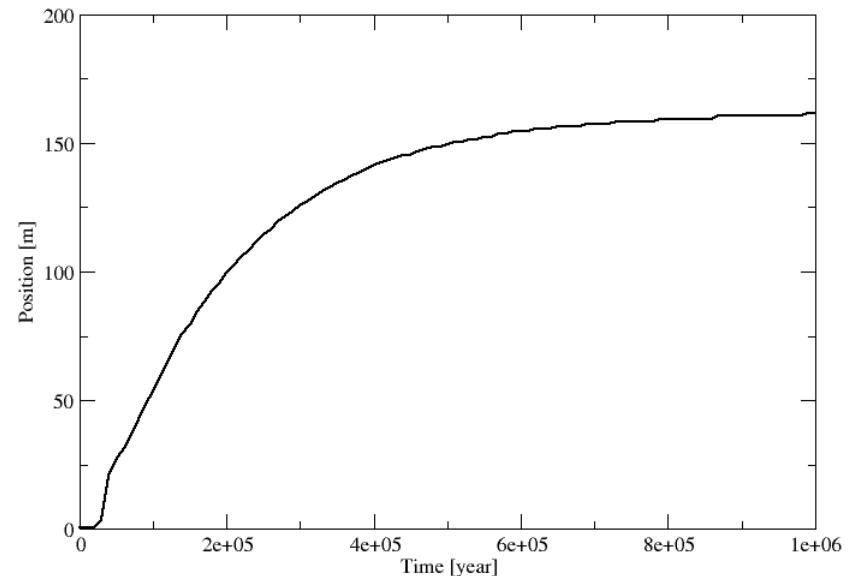
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Timeseries of gas saturation in the injection cell



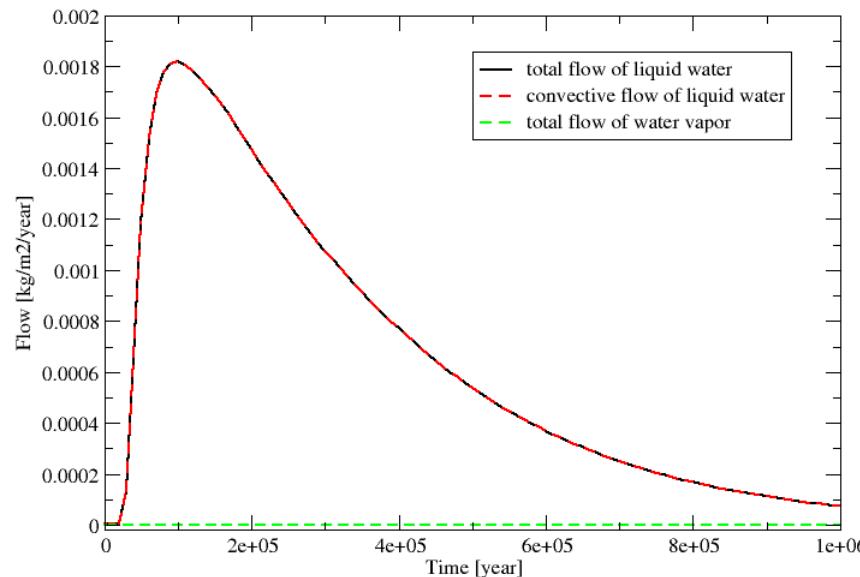
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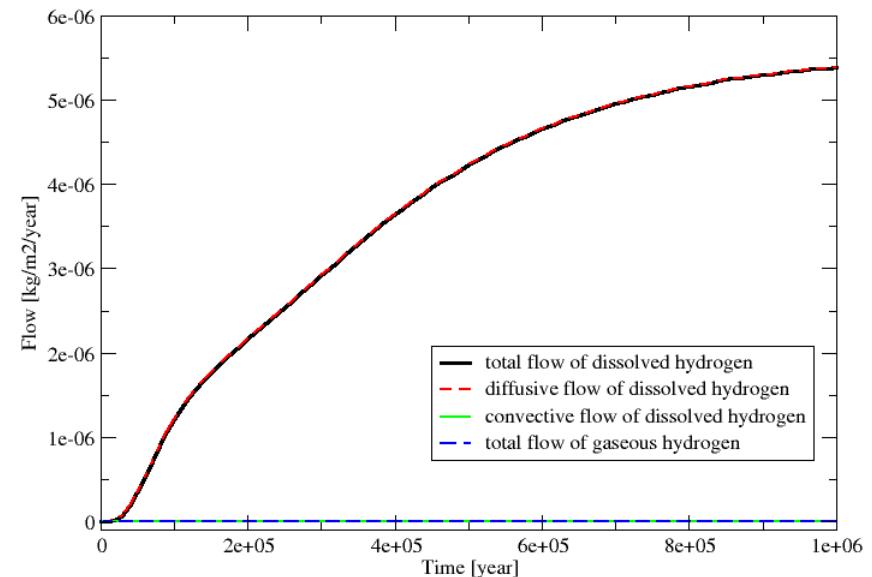
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Timeseries of hydrogen flow across exit boundary

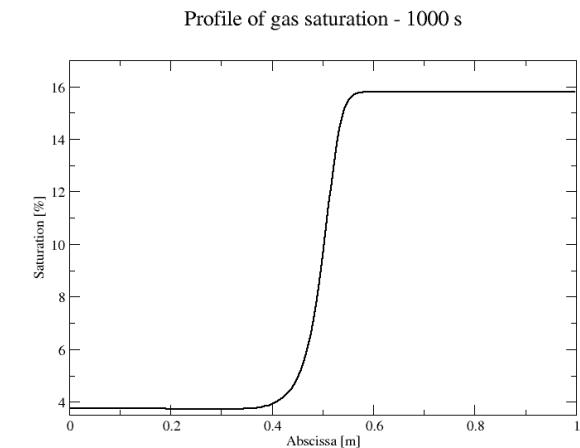
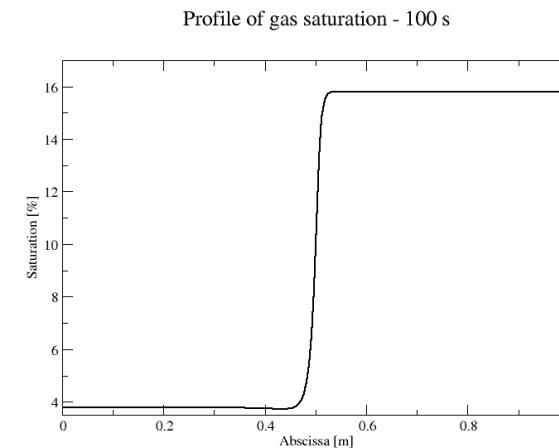
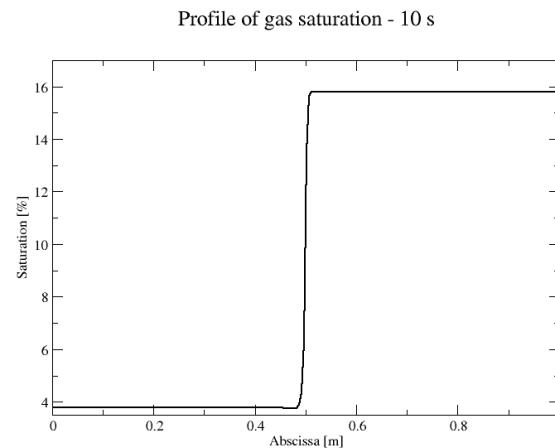
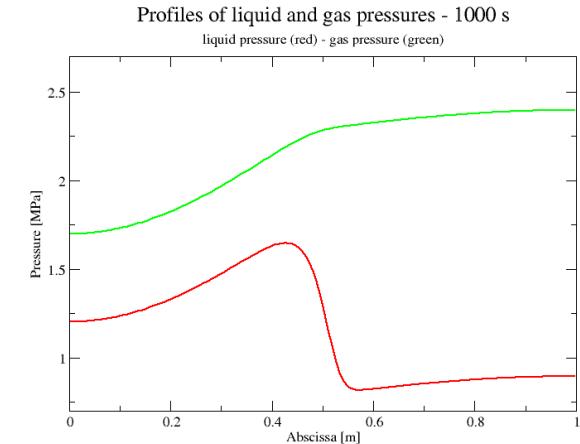
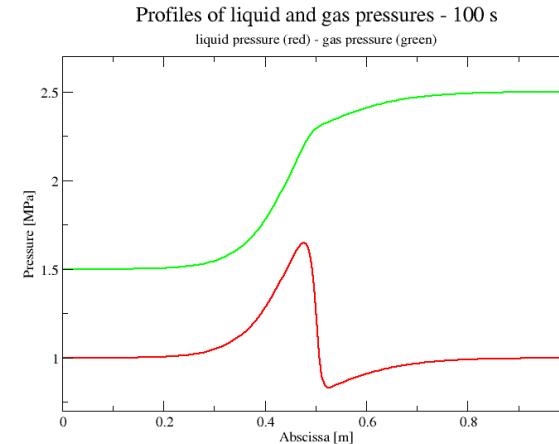
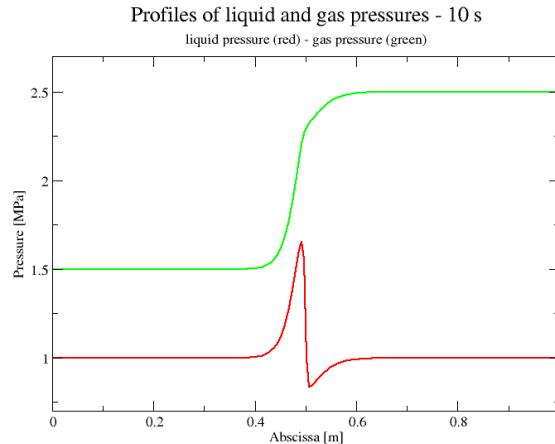


## Problem 3: two-phase flow with non equilibrium states at initial time

- Regular spatial discretization:  $dx=0.005$  m
- Time discretization:
  - »  $dt_{min}=1$  s,  $dt_{max} = 1000$  years
- Relative convergence criterion:  $10^{-5}$

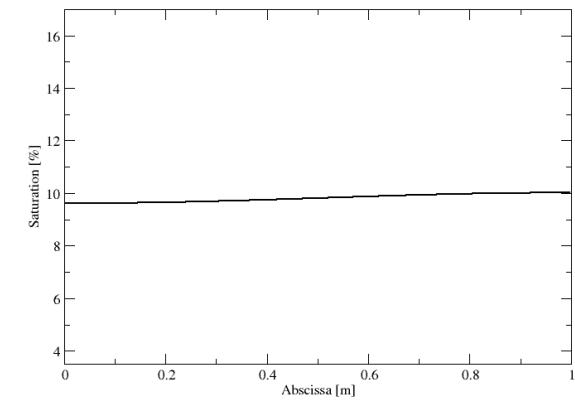
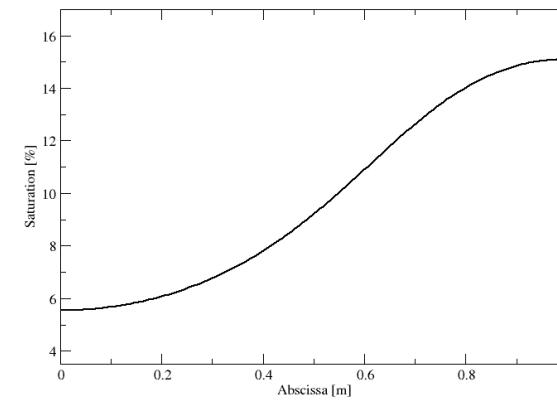
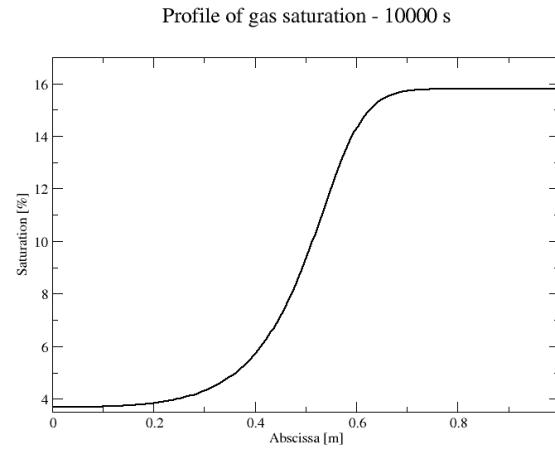
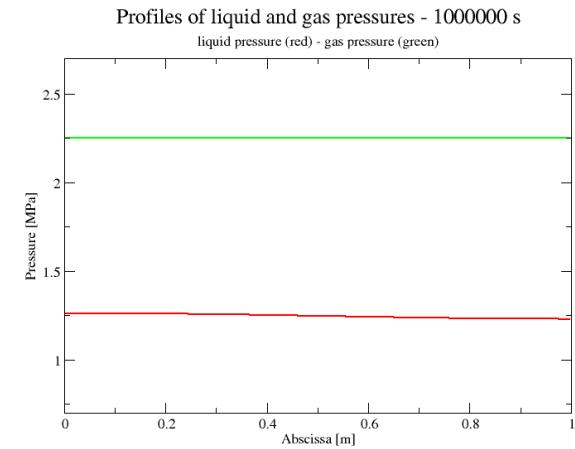
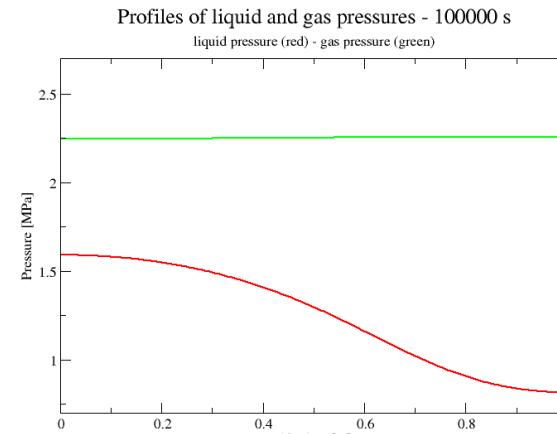
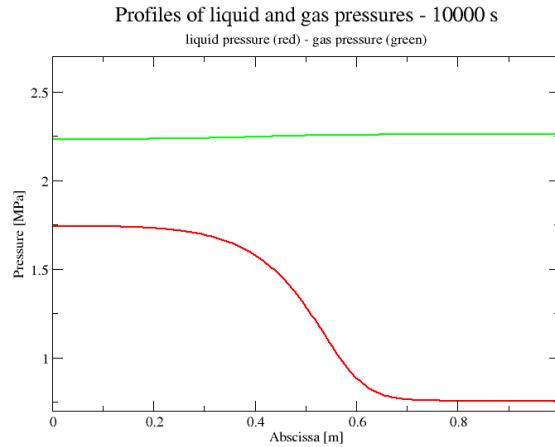
# Problem 3: two-phase flow with non equilibrium states at initial time

## ➤ Two adjacent partially saturated zones at initial time



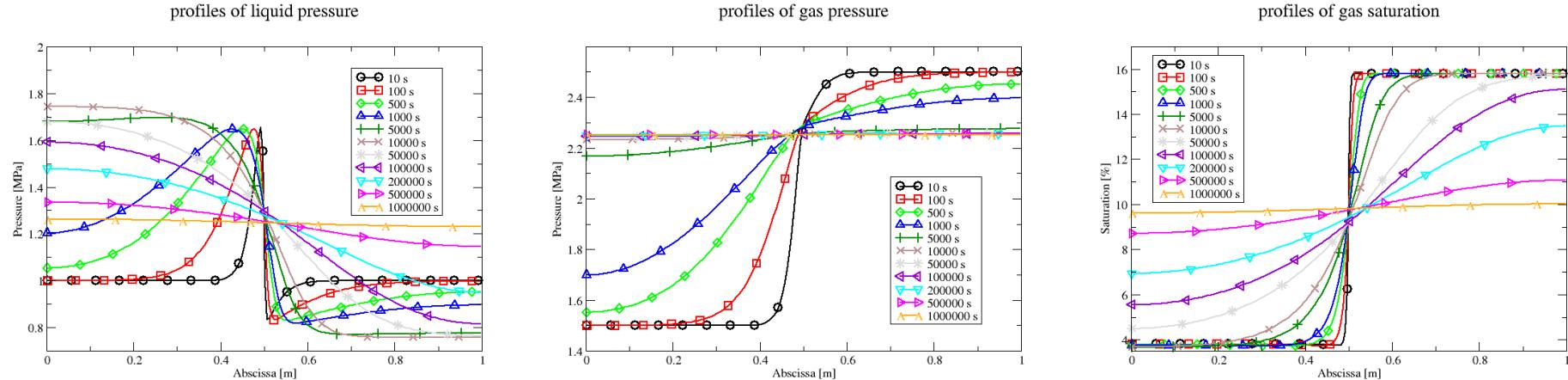
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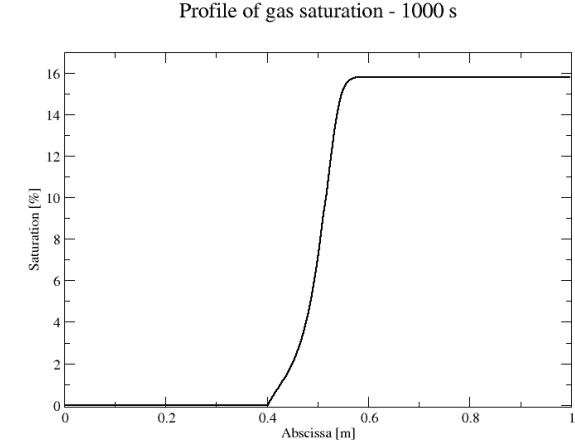
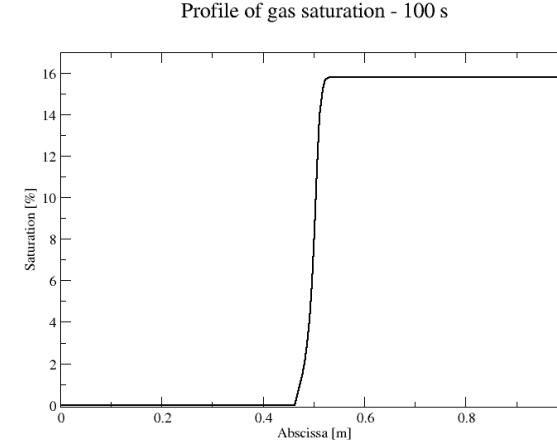
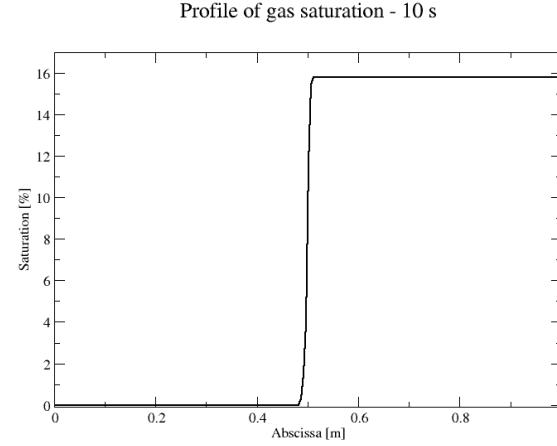
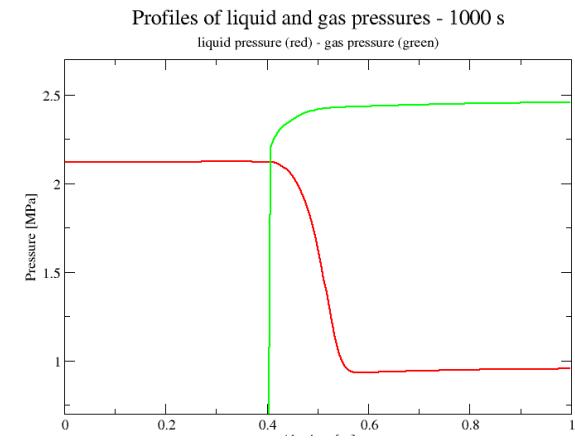
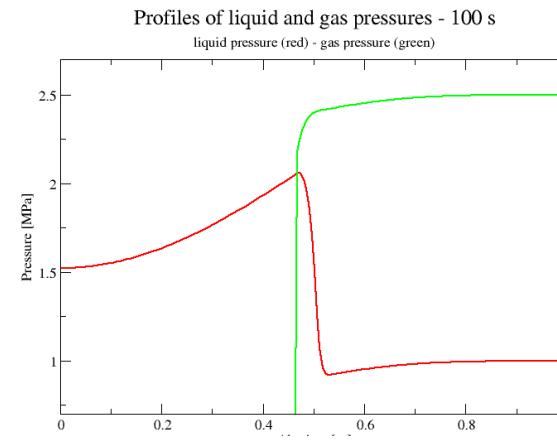
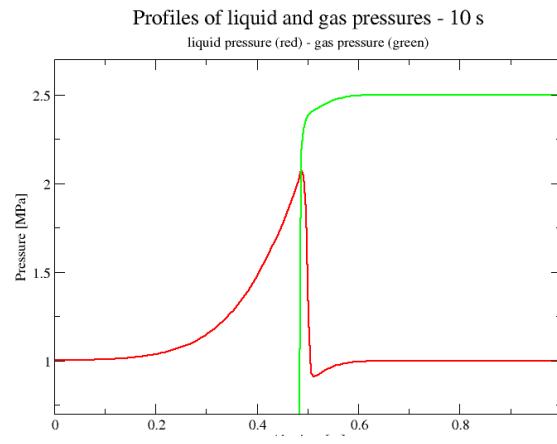
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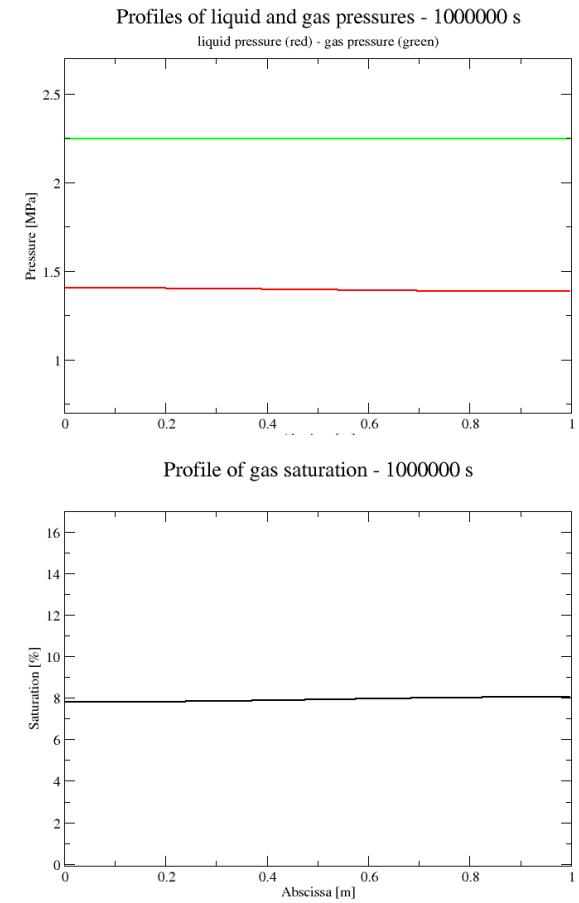
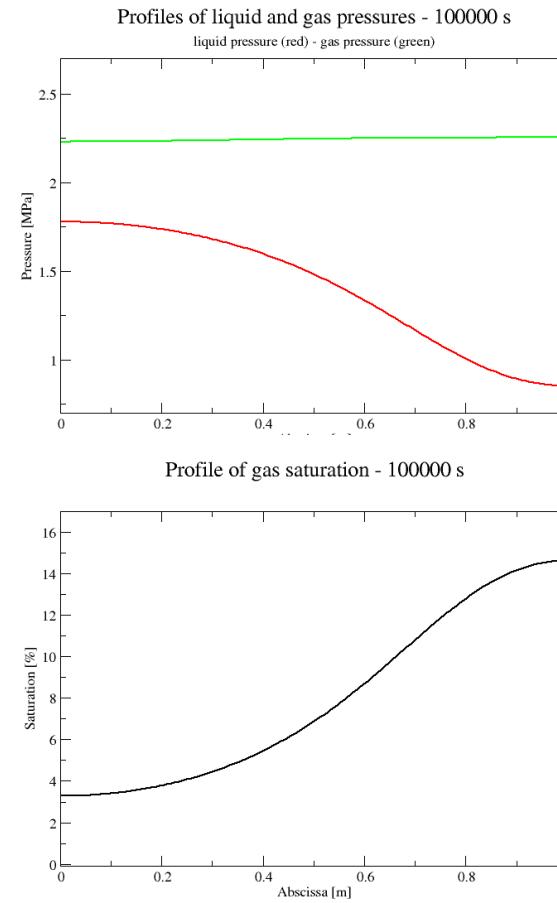
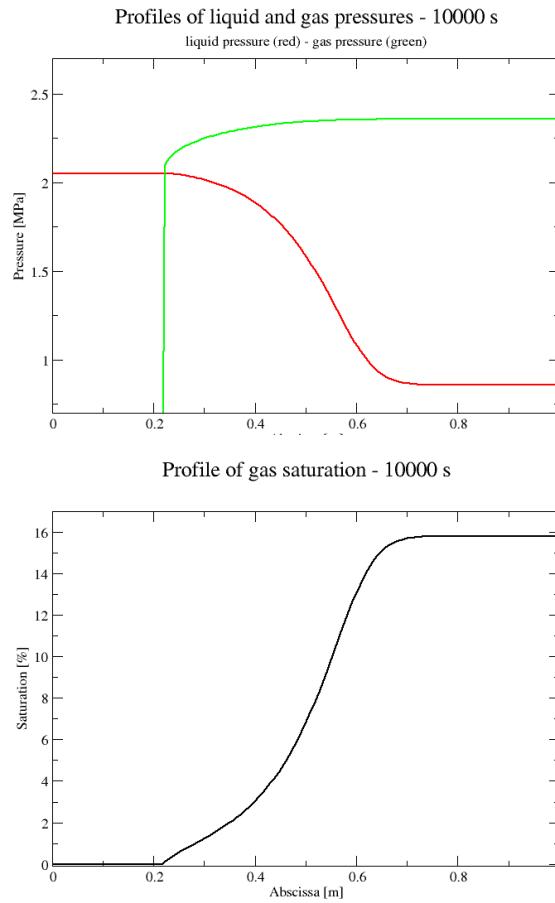
# Problem 3: two-phase flow with non equilibrium states at initial time

➤ Left zone is fully liquid saturated at initial time



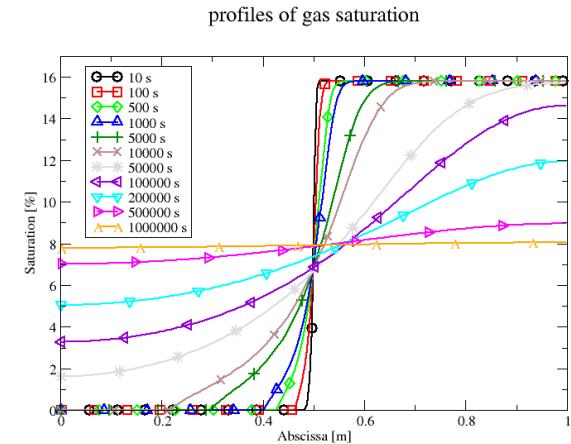
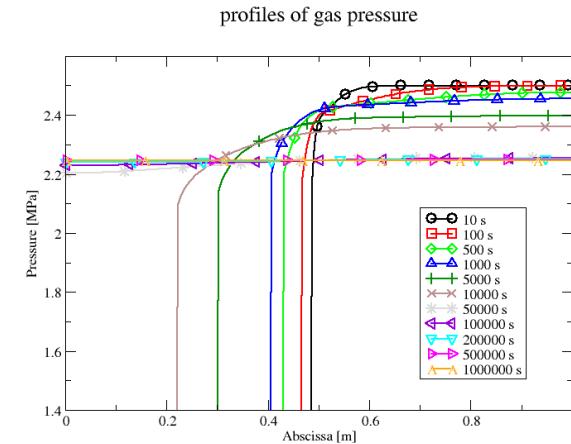
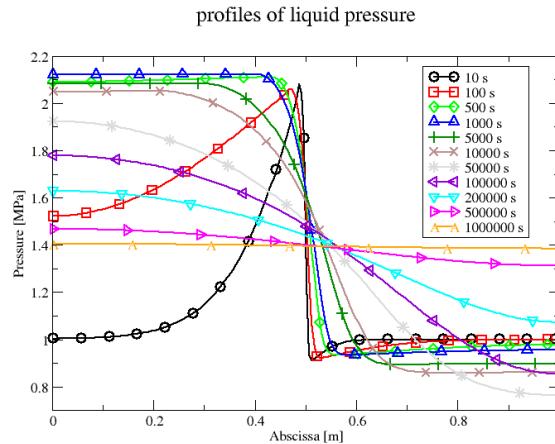
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➤ Left zone is fully liquid saturated at initial time



# Problem 3: two-phase flow with non equilibrium states at initial time

➤ Left zone is fully liquid saturated at initial time



# Problem 4: two-phase flow with non equilibrium states at initial time

- **Irregular spatial discretization:**
  - »  $\text{dxmax}=2.25 \text{ cm}$ ,  $\text{dxmin}=0.02 \text{ cm}$
- **Time discretization:**
  - »  $\text{dtmin}=10 \text{ s}$ ,  $\text{dtmax} = 100 \text{ s}$
- **Relative convergence criterion:  $10^{-5}$**

